
(12) UK Patent Application (19) GB (11) 2 077 289 A

(21) Application No 8117148

(22) Date of filing 4 Jun 1981

(30) Priority data

(31) 8003313

(32) 6 Jun 1980

(33) Netherlands (NL)

(43) Application published
16 Dec 1981

(51) INT CL³

C07C 1/04 // B01J 23/74

(52) Domestic classification

C5E 283 332 386 391 CD

B1E 1162 1180 1285

1298 1315 1382 1462

1701 1712 1714 1719

1721 AD

(56) Documents cited

None

(58) Field of search

B1E

C5E

(71) Applicants

Shell Internationale

Research Maatschappij

B.V.,

Carel van Bylandtlaan 30,

The Hague, The

Netherlands, Holland

(72) inventors

Henricus Michael Joseph

Bijwaard,

Micheal Adriaan Maria

Boersma,

Swan Tiong Sie

(74) Agent

R. C. Rogers,

4 York Road, London

SE1 7NA

(54) A process for the preparation of middle distillates

(57) Middle distillates are prepared by a catalytic hydrotreatment of a heavy product which has been obtained by conversion of syngas with a H₂/CO

mol. ratio of at least 1.5 over a SiO₂-supported Zr, Ti or Cr-promoted Co-catalyst of specified composition. This catalyst has been prepared by impregnation and has been calcined and then reduced at a low temperature.

GB 2 077 289 A

SPECIFICATION**A process for the preparation of middle distillates**

The invention relates to a process for the preparation of middle distillates from a mixture of carbon monoxide and hydrogen.

5 The preparation of hydrocarbons from an H₂/CO mixture by contacting said mixture at elevated temperature and pressure with a catalyst is known in the literature as the Fischer-Tropsch hydrocarbon synthesis process. Catalysts frequently used for this purpose contain one or more metals of the iron group together with one or more promoters and sometimes a carrier material. The preparation of Fischer-Tropsch catalysts can in principle be carried out in three manners, namely by precipitation, melting or impregnation. Both the precipitation route and the melting route are not very attractive 5 preparation methods for the Fischer-Tropsch catalysts since their reproducibility is low. The precipitation route is moreover very time-consuming, and the melting route requires much energy. Also, the catalytic properties of the catalysts prepared by melting and precipitation, in particular activity and stability, are often not entirely satisfactory. A much more attractive preparation method for the Fischer- 10 Tropsch catalysts is the impregnation route. This is simple to carry out, yields well-reproducible results and generally leads to catalysts having high activity and stability. Briefly, the impregnation route amounts to impregnating a porous carrier with one or more aqueous solutions of salts of one or more metals of the iron group and of one or more promoters, followed by drying, calcining and reducing the 15 composition. As promoters for the catalysts prepared by impregnation, many elements are suitable, such as alkali metals, alkaline earth metals, metals of Group VIB, Ti, Zr, Th, V, Mn and Cu. As carrier materials for the catalysts prepared by impregnation both amorphous and crystalline materials are suitable. Suitable carriers are, for example, silica, alumina, zirconia, thoria, boria and combinations thereof, such as silica-alumina and silica-magnesia, and zeolites such as mordenite, faujasite and zeoliteomega. 20

25 The Applicant has carried out an extensive investigation into the preparation of hydrocarbons from H₂/CO mixtures using Fischer-Tropsch catalysts prepared by impregnation. This investigation revealed that the behaviour of these catalysts in said conversion greatly depends on the following factors:

- 1) the nature of the metal of the iron group and the load used,
- 2) the nature of the promoter and the load used,
- 30 3) the nature of the carrier and
- 4) the temperature treatment used.

It was further found that the use of these catalysts usually results in a product having a very broad molecular weight distribution and that only a small part of said product consists of middle distillates. In addition to the yield, the pour point of said middle distillates is also unsatisfactory. In this connection the 35 direct conversion of H₂/CO mixtures by the Fischer-Tropsch process is a not very attractive route for the preparation of middle distillates on a technical scale.

By "middle distillates" are meant in this patent application hydrocarbon mixtures the boiling range of which mainly corresponds with that of the kerosine and gasoil fractions obtained in the conventional atmospheric distillation of crude oil. In said distillation the following fractions are consecutively 40 separated from the crude oil: one or more gasoline fractions with a boiling range between 30 and 200°C, one or more kerosine fractions with a boiling range between 140 and 300°C and one or more gasoil fractions with a boiling range between 180 and 370°C.

Further investigation by the Applicant into the preparation of middle distillates from H₂/CO mixtures revealed that in the conversion of H₂/CO mixtures with the use of catalysts prepared by 45 impregnation, a product is obtained which is very valuable for the preparation of middle distillates, if the catalysts contain 10—40 parts by weight of cobalt and 0.25—5 parts by weight of zirconium, titanium or chromium per 100 parts by weight of silica and have been calcined at a temperature of 350—700°C and reduced at a temperature of 200—350°C. For it has been found that the high-boiling part of the product thus obtained can be converted in high yield into middle distillates by a catalytic 50 hydrotreatment. The feed chosen for hydrotreatment is at least that part of the reaction product the initial boiling point of which is higher than the final boiling point of the heaviest middle distillate required as final product. The hydrotreatment which is characterized by a very low hydrogen consumption yields middle distillates having a considerably better pour point than those obtained in the direct conversion of an H₂/CO mixture by the Fischer-Tropsch process.

55 For brevity's sake catalysts containing 10—40 parts by weight of cobalt and 0.25—5 parts by weight of zirconium, titanium or chromium per 100 parts by weight of silica and prepared by impregnating a silica carrier with one or more aqueous solutions of salts of cobalt and zirconium, titanium or chromium, followed by drying the composition, calcining at 350—700°C and reducing at 200—350°C, will be further referred to in this patent application as "Co-impregnation catalysts".

60 If the feed to be converted over the Co-impregnation catalyst has an H₂/CO molar ratio of less than 1.5, water has to be added to said feed and the Co-impregnation catalyst must be used in combination with a CO-shift catalyst.

The present patent-application therefore relates to a process for the preparation of middle distillates from a mixture of carbon monoxide and hydrogen, in which process an H₂/CO-containing feed

- is contacted in a first stage with a Co-impregnation catalyst at elevated temperature and pressure, with the proviso that if the feed has an H₂/CO molar ratio of less than 1.5, water is added to said feed and that the Co-impregnation catalyst is used in combination with a CO-shift catalyst, and that of the reaction product of the first stage at least that part of the initial boiling point of which is higher than the final boiling point of the heaviest middle distillate required as final product is subjected in a second stage to a catalytic hydrotreatment. 5
- If the feed for the first stage of the process according to the invention has an H₂/CO molar ratio of less than 1.5, water has to be added to this feed and the Co-impregnation catalyst must be used in combination with a CO-shift catalyst. Preference is given to the use of CO-shift catalysts containing copper and zinc in which the Cu/Zn atomic ratio lies between 0.25 and 4.0. The excellent properties of the Co-impregnation catalysts used in the first stage of the process according to the invention, which catalysts can among other things be used at substantially higher pressures than the usual Fischer-Tropsch cobalt catalysts, enable a reaction product obtained by contacting an H₂- and CO-containing feed to which water is added with a CO-shift catalyst, to be converted over the Co-impregnation catalyst without CO₂ being removed from said product. Feeds with an H₂/CO molar ratio of less than 1.5 and, if desired, also feeds having an H₂/CO molar ratio of at least 1.5 can also be processed in the first stage of the process of the invention by contacting them after the addition of water with either a catalyst bed built up of several layers of consecutively a CO-shift catalyst and a Co-impregnation catalyst, or a physical mixture of a CO-shift catalyst and a Co-impregnation catalyst. 10
- If in the process according to the invention, either as feed for the first stage or in the preparation of the feed for the first stage, use is made of an H₂- and CO-containing mixture to which water has been added and which mixture is contacted with a catalyst or catalyst combination possessing CO-shift activity, the quantity of water to be added to the H₂- and CO-containing mixture is mainly determined by the H₂/CO molar ratio of the mixture, the CO-shift activity of the catalyst or catalyst combination and the desired H₂/CO molar ratio of the product that is converted over Co-impregnation catalyst. The H₂- and CO-containing mixture used as feed for the first stage of the process according to the invention can, for example, be obtained by steam gasification of carbon-containing material. A very suitable feed for the first stage of the process according to the invention is a carbon monoxide- and hydrogen-containing fraction which can be separated from a reaction product that is obtained if an H₂/CO mixture (1) with an H₂/CO molar ratio of less than 2.0 is contacted with a bifunctional catalyst combination containing one or more metal components having catalytic activity for the conversion of an H₂/CO mixture into acyclic hydrocarbons and/or acyclic oxygen-containing hydrocarbons and a crystalline silicate having the capacity of catalysing the conversion of acyclic hydrocarbons and acyclic oxygen-containing hydrocarbons into aromatic hydrocarbons, with the proviso that if the H₂/CO mixture (1) has an H₂/CO molar ratio of less than 1.5, a trifunctional catalyst combination is used containing one or more metal components with catalytic activity for the conversion of an H₂/CO mixture into acyclic hydrocarbons and/or acyclic oxygen-containing hydrocarbons, one or more metal components with CO-shift activity and a crystalline silicate having the capacity of catalysing the conversion of acyclic hydrocarbons and acyclic oxygen-containing hydrocarbons into aromatic hydrocarbons. Said crystalline silicates are characterized in that they possess the following properties after one hour's calcination in air at 500°C: 20
- a) thermally stable to a temperature above 600°C,
 b) an X-ray powder diffraction pattern containing the four lines stated in table A as strongest lines. 25
- 30
- 35
- 40

Table A

d(Å)	Relative intensity
11,1 ± 0,2	VS
10,0 ± 0,2	VS
3,84 ± 0,07	S
3,72 ± 0,06	S

- where the letters have the following meanings:
- VS = very strong; S = strong, and
 c) in the formula representing the composition of the silicate expressed in moles of oxides and containing in addition to oxides of hydrogen, alkali metal and/or alkaline earth metal and silicon, one or more oxides of a trivalent metal A chosen from the group consisting of aluminium, iron, gallium, rhodium, chromium and scandium, the SiO₂/A₂O₃ molar ratio is more than 10. 45
- The bi- and trifunctional catalyst combinations referred to above contain, in addition to metal components with catalytic activity, a crystalline metal silicate characterized by the properties stated in a) to c). Preference is given to a silicate containing only one of said metals and in particular to silicates 50

containing as metal aluminium, iron or gallium. The complete X-ray powder diffraction pattern of a typical example of a silicate as described above is shown in table B.

Table B

d(Å)	Relative intensity	d(Å)	Relative intensity
11,1	100	4,00	3
10,0	70	3,84	57
8,93	1	3,72	31
7,99	1	3,64	10
7,42	1	3,44	5
6,68	7	3,34	3
6,35	11	3,30	5
5,97	18	3,25	2
5,70	7	3,05	5
5,56	10	2,98	12
5,35	2	2,96	3
4,98	6	2,86	2
4,60	4	2,73	2
4,35	5	2,60	2
4,25	7	2,48	3
4,07	2	2,40	2

Although the trifunctional catalyst combinations are described in the present patent application as catalyst combinations containing one or more metal components with catalytic activity for the conversion of an H₂/CO mixture into acyclic hydrocarbons and/or acyclic oxygen-containing hydrocarbons and one or more metal components with CO-shift activity, this by no means implies that separate metal components each individually possessing one of the two catalytic functions must be present in the trifunctional catalyst combinations. It has in fact been found that metal components and combinations of metal components having catalytic activity for the conversion of an H₂/CO mixture into substantially acyclic oxygen-containing hydrocarbons usually also have sufficient CO-shift activity, so that in this case it will usually suffice to introduce one metal component or one combination of metal components into the trifunctional catalyst combinations. Metal components and combinations of metal components having catalytic activity for the conversion of an H₂/CO mixture into substantially acyclic hydrocarbons usually possess no or insufficient CO-shift activity. Consequently, when such metal components or metal component combinations are used in the trifunctional catalyst combinations one or more separate metal components with CO-shift activity must mostly be introduced into the catalyst combination.

The crystalline silicate-containing bi- and trifunctional catalyst combinations referred to above preferably consist of two or three separate catalysts that are indicated for the sake of convenience as catalysts X, Y and Z. Catalyst X is the catalyst containing the metal components with catalytic activity for the conversion of an H₂/CO mixture into acyclic hydrocarbons and/or acyclic oxygen-containing hydrocarbons. Catalyst Y is the crystalline silicate. Catalyst Z is the catalyst containing the metal components with CO-shift activity. As explained in the foregoing, in the case of the trifunctional catalyst combinations the use of a catalyst Z can be dispensed with in a number of cases.

If as catalyst X use is made of a catalyst which is capable of converting an H₂/CO mixture into substantially acyclic oxygen-containing hydrocarbons, preference is given to a catalyst capable of

converting the H₂/CO mixture into substantially methanol and/or dimethyl ether. Very suitable catalysts for this purpose are ZnO—Cr₂O₃ compositions, in particular such compositions in which the atomic percentage of zinc based on the sum of zinc and chromium is at least 60% and preferably 60—80%. If the catalyst X used is a ZnO—Cr₂O₃ composition, the use of a catalyst Z can be dispensed with in the trifunctional catalyst combinations.

The following iron catalysts are also very suitable as catalysts X:

a) catalysts containing 30—75 parts by weight of iron and 5—40 parts by weight of magnesium per 100 parts by weight of alumina and prepared by impregnating an alumina carrier with one or more aqueous solutions of salts of iron and of magnesium followed by drying the composition, calcining it at a temperature of 700—1200°C and reducing it. Particularly preferred are catalysts of this type that contain in addition to 40—60 parts by weight of iron and 7.5—30 parts by weight of magnesium, 0.5—5 parts by weight of copper as reduction promoter and 1—5 parts by weight of potassium as selectivity promoter per 100 parts by weight of alumina and which are calcined at 750—850°C and reduced at 250—350°C.

b) Catalysts containing 10—40 parts by weight of iron and 0.25—10 parts by weight of chromium per 100 parts by weight of silica and prepared by impregnating a silica carrier with one or more aqueous solutions of salts of iron and of chromium followed by drying and calcining the composition and reducing it at a temperature of 350—750°C. Particular preference is given to catalysts of this type that contain in addition to 20—35 parts by weight of iron and 0.5—5 parts by weight of chromium, 1—5 parts by weight of potassium as selectivity promoter and which are calcined at 350—700°C and reduced at 350—500°C.

When the iron catalysts mentioned under a) and b) are used as catalyst X, the use of a catalyst Z can be dispensed with in the trifunctional catalyst combinations.

In the crystalline silicate-containing bi- and trifunctional catalyst combinations the catalysts X, Y and possibly Z are preferably present as a physical mixture. When a fixed catalyst bed is used, the bed can also be built up of alternating layers of particles of catalysts X, Y and possibly Z.

If in the process according to the invention the feed used for the first stage is a carbon monoxide- and hydrogen-containing fraction separated from the reaction product that can be obtained by contacting an H₂/CO mixture (1) with the above-mentioned crystalline silicate-containing bi- or trifunctional catalyst combinations, for said purpose a fraction is preferably chosen such as is separated from a reaction product prepared under the following conditions: a temperature of 200—500°C, in particular 250—450°C, a pressure of 1—150 bar, in particular 5—100 bar, and a space velocity of 50—5000, in particular 300—3000 NI of gas/l of catalyst/h.

Another very suitable feed for the first stage of the process according to the invention is a carbon monoxide- and hydrogen-containing fraction that can be separated from a reaction product that is obtained if an H₂/CO mixture with an H₂/CO molar ratio of less than 1.0 is contacted with an iron-containing bifunctional catalyst or catalyst combination possessing CO-shift activity in addition to activity for the conversion of an H₂/CO mixture into substantially hydrocarbons. For this purpose use is preferably made of a bifunctional catalyst prepared by impregnation and containing iron on a carrier. Examples of such catalysts are the iron catalysts described in the foregoing under a) and b). If in the process according to the invention the feed for the first stage is a carbon monoxide- and hydrogen-containing fraction separated from the reaction product that can be obtained by contacting an H₂/CO mixture (2) with the above-mentioned iron-containing bifunctional catalyst or catalyst combination, for said purpose a fraction is preferably chosen such as is separated from a reaction product prepared under the following conditions: a temperature of 200—350°C and in particular of 250—350°C, a pressure of 10—70 bar and in particular of 20—50 bar and a space velocity of 500—5000 and in particular of 500—2500 NI of gas/l of catalyst/h.

If in the process according to the invention the feed used for the first stage is an H₂- and CO-containing fraction separated from the reaction product obtained either by contacting an H₂/CO mixture (1) with the above-mentioned crystalline silicate-containing bi- or trifunctional catalyst combinations, or by contacting an H₂/CO mixture (2) with the above iron-containing bifunctional catalyst or catalyst combinations, said fraction can contain, in addition to carbon monoxide and hydrogen, also other components of the reaction product. It is possible, for example, to use as feed for the first stage of the process according to the invention the C₂⁻ fraction or C₄⁻ fraction of the reaction product or even the complete reaction product. The above-mentioned H₂/CO mixtures (1) and (2) are preferably obtained by steam gasification of coal at a temperature of 900—1500°C and a pressure of 10—100 bar.

The first step of the process according to the invention is preferably carried out at a temperature of 125—350°C, in particular 175—275°C, and a pressure of 1—150 bar, in particular 5—100 bar.

In the process according to the invention at least that part of the reaction product of the first stage the initial boiling point of which is higher than the final boiling point of the heaviest middle distillate required as final product must be subjected to a catalytic hydrotreatment in a second stage. The catalytic hydrotreatment is carried out by contacting the relevant fraction of the reaction product of the first stage with a catalyst containing one or more metals with hydrogenation activity on a carrier, at elevated temperature and pressure and in the presence of hydrogen. Examples of suitable catalysts are sulphidic catalysts containing nickel and/or cobalt and moreover molybdenum and/or tungsten on a

carrier such as alumina or silica-alumina. In the catalytic hydrotreatment use is preferably made of a catalyst containing one or more noble metals of Group VIII on a carrier. The quantity of noble metal present on the carrier may vary within wide limits, but is usually 0.05—5% by weight. The noble metals of Group VIII, which may be supported on the carrier, are platinum, palladium, rhodium, ruthenium, 5 iridium and osmium, of which platinum is preferred. If desired, two or more of said metals may be present in the catalysts. The quantity of noble metal of Group VIII present in the catalyst is preferably 0.1—2% by weight and in particular 0.2—1% by weight. Examples of suitable carriers for the noble metal catalysts are amorphous oxides of the elements of Groups II, III and IV, such as silica, alumina, magnesia, zirconia as well as mixtures of said oxides such as silica-alumina, silica-magnesia and silica-zirconia and zeolitic materials such as mordenite and faujasite. As carriers for the noble metal catalysts 10 alumina and silica-alumina are preferred. A very suitable noble metal catalyst for the present purpose is a catalyst containing one or more noble metals of Group VIII on a carrier, which carrier comprises 13—15% by weight of alumina, the remainder being silica. Suitable conditions for carrying out the catalytic hydrotreatment are a temperature of 175—400°C, a hydrogen partial pressure of 10—250 15 bars, a space velocity of 0.1—5 kg.l⁻¹.h⁻¹ and a hydrogen/oil ratio of 100—5000 Nl.kg⁻¹. The catalytic hydrotreatment is preferably carried out under the following conditions: a temperature of 250—350°C, a hydrogen partial pressure of 25—150 bars, a space velocity of 0.25—2 kg.l⁻¹.h⁻¹ and a hydrogen/oil ratio of 250—2500 Nl.kg⁻¹. By making a correct choice of the catalyst and the treating 20 conditions in the second stage it is possible in the process according to the invention to prepare, in addition to middle distillate, high-viscosity index lubricating oil from a heavy fraction of the product of the first stage.

The invention will now be illustrated with reference to the following Example.

EXAMPLE

In the investigation use was made of the following catalysts:

25 Catalyst 1

Co/Zr/SiO₂ catalyst containing 25 parts by weight of cobalt and 1.8 parts by weight of zirconium per 100 parts by weight of silica, which was prepared by impregnating a silica carrier with an aqueous solution containing a cobalt and a zirconium salt, followed by drying the composition, calcining at 500°C and reducing at 280°C.

30 Catalyst 2

Pt/SiO₂—Al₂O₃ catalyst, containing 0.82 parts by weight of platinum per 100 parts by weight of carrier, which carrier consisted of 14.6% by weight of alumina and 85.4% by weight of silica.

Catalyst 3

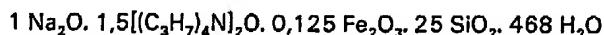
Cu/Zn/Al₂O₃ catalyst having a Cu/Zn atomic ratio of 0.55.

35 Catalyst 4

ZnO—Cr₂O₃ catalyst in which the atomic percentage of zinc, based on the sum of zinc and chromium, was 70%.

Catalyst 5

A crystalline silicate A was prepared by heating a mixture of SiO₂, NaOH, (C₃H₇)₄NOH and 40 Fe(NO₃)₃ in water with the molar composition



at 150°C for 6 hours in an autoclave under autogenous pressure. After the reaction mixture had been cooled, the silicate A formed was filtered off, washed with water until the pH of the washing water was about 8, dried at 120°C and calcined at 500°C. Silicate A had the following properties:

- 45 a) thermally stable to a temperature above 800°C,
- b) an X-ray powder diffraction pattern mainly as stated in table B,
- c) an SiO₂/Fe₂O₃ molar ratio of 200.

Catalyst 5 was prepared from silicate A by boiling silicate A with 1.0 molar NH₄NO₃ solution, washing with water, reboiling with 1.0 molar NH₄NO₃ solution, washing, drying and calcining.

50 Catalyst 6

Fe/Mg/Cu/K/Al₂O₃ catalyst containing 50 parts by weight of iron, 20 parts by weight of magnesium, 2.5 parts by weight of copper and 4 parts by weight of potassium per 100 parts by weight of alumina, which catalyst had been prepared by impregnating an alumina carrier with an aqueous solution containing an iron, magnesium, copper and potassium salt, followed by drying the

55 composition, calcining at 800°C and reducing at 325°C.

5

10

15

20

25

30

35

40

45

50

55

Catalyst mixture I

Catalyst mixture I consisted of a layer of catalyst 3 and a layer of catalyst 1 in a volume ratio of 1:2.

Catalyst mixture II

- 5 Catalyst mixture II consisted of a physical mixture of catalyst 4 and catalyst 5 in a volume ratio 5 2:1.

The catalysts 1, 2, 3 and 6 and the catalyst mixtures I and II were tested in the preparation of middle distillates from H₂- and CO-containing mixtures.

Experiment 1

- 10 An H₂/CO mixture with an H₂/CO molar ratio of 1.8 was passed through a 250-ml reactor containing a fixed catalyst bed consisting of 45 ml of catalyst 1, at a temperature of 220°C, a pressure of 30 bar and a space velocity of 500 Nl.l⁻¹.h⁻¹. The conversion of the H₂/CO mixture was 93% by volume. The reaction product prepared over catalyst 1 is indicated as product 1A. 10

Experiment 2

- 15 An H₂/CO mixture with an H₂/CO molar ratio of 0.5 was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 10 ml of catalyst 3, with the addition of 268 ml of water/l of catalyst/h at a temperature of 220°C, a pressure of 30 bar and a space velocity of 1000 Nl.l⁻¹.h⁻¹. The reaction product prepared over catalyst 3, the H₂/CO molar ratio of which was 2.0, was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 27 ml of catalyst 1, at a temperature of 220°C, a 20 pressure of 30 bar and a space velocity of 500 Nl.l⁻¹.h⁻¹. The conversion of the H₂/CO mixture was 93% by volume. 20

The reaction product prepared over catalyst 1 is indicated as product 2A.

Experiment 3

- An H₂/CO mixture with an H₂/CO molar ratio of 0.5 was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 15 ml of catalyst mixture I, with the addition of 268 ml of water/l of catalyst/h at a temperature of 220°C; a pressure of 30 bar and a space velocity of 500 Nl.l⁻¹.h⁻¹. The conversion of the H₂/CO mixture was 90% by volume. The reaction product prepared over catalyst mixture I is indicated as product 3A. 25

Experiment 4

- 30 An H₂/CO mixture with an H₂/CO molar ratio of 1.3 was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 3.75 ml of catalyst mixture II, at a temperature of 375°C and a pressure of 60 bar. The reaction product prepared over catalyst mixture II, the H₂/CO molar ratio of which was 2.0, was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 11.25 ml of the catalyst 1, at a temperature of 220°C and a pressure of 60 bar. In this experiment the space 35 velocity based on the total catalyst system (catalyst mixture II + catalyst 1) was 500 Nl.l⁻¹.h⁻¹. The reaction product prepared over catalyst 1 is indicated as product 4A. 35

Experiment 5

- An H₂/CO mixture with an H₂/CO molar ratio of 0.5 was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 5 ml of catalyst 6, at a temperature of 280°C and a pressure of 30 bar. 40 The reaction product prepared over catalyst 6, the H₂/CO molar ratio of which was 0.41, was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 5 ml of catalyst mixture I, with the addition of 241 ml of water/l of catalyst/h at a temperature of 230°C and a pressure of 30 bar. In this experiment the space velocity based on the total catalyst system (catalyst 6 + catalyst mixture I) was 1000 Nl.l⁻¹.h⁻¹. The reaction product prepared over catalyst mixture I is indicated as product 5A. 45 The composition of products 1A—5A was determined by separating samples of these products by distillation into a 150°C⁺ fraction, a 150—250°C fraction, a 250—360°C fraction, a 360—400°C fraction and a 400°C⁺ fraction and separating the latter fraction by cooling to -20°C in the presence of a mixture of methyl ethyl ketone and toluene into a 400°C⁺ oil fraction and a 400°C⁺ paraffin fraction. The composition of the products 1A—5A is stated in table C. Of each of the products 1A—5A the C₅⁺ 50 fraction was passed through a 50-ml reactor containing a fixed catalyst bed consisting of 8 ml of catalyst 2, at a temperature of 345°C, a hydrogen partial pressure of 130 bar, a space velocity of 1.25 l.l⁻¹.h⁻¹ and a hydrogen/oil ratio of 2000 Nl/l. The reaction products prepared over catalyst 2 are indicated as products 1B—5B, respectively. The composition of the products 1B—5B, which was determined in the same manner as that of products 1A—5A, is stated in table C.

Table C

Product composition, % by wt

Product No.		1A	1B	2A	2B	3A	3B	4A	4B	5A	5B
fraction	150°C-	4,2	6,9	4,3	7,0	6,3	9,0	19,3	22,3	10,1	13,2
fraction	150—250°C	18,7	22,3	18,6	22,0	20,6	24,2	23,1	28,6	22,3	27,8
fraction	250—360°C	24,9	44,7	25,0	44,6	27,0	46,6	18,6	32,0	23,1	39,3
fraction	360—400°C	10,4	11,0	10,3	10,9	9,2	8,9	7,8	7,5	9,3	8,2
oil fraction	400°C+	3,1	10,6	3,1	10,8	2,9	9,0	2,3	6,2	2,8	6,8
paraffin fraction	400°C+	38,7	4,5	38,7	4,5	34,0	2,3	28,9	3,4	32,4	4,7

Some properties of three fractions of product 1B are stated below:

Fraction 150—250°C	smoke point >50 mm cloud point -35°C pour point -32°C	5	5
Fraction 250—360°C	cloud point -4°C pour point -1°C diesel index 102		
Oil fraction 400°C+	$V_{K_{100}}$ 31,3 cS		
10	$V_{K_{210}}$ 62,2 cS		10
	VI 152,7		

CLAIMS

1. A process for the preparation of middle distillates from a mixture of carbon monoxide and hydrogen, characterized in that an H₂- and CO-containing feed is contacted in a first stage at elevated temperature and pressure with a catalyst containing 10—40 parts by weight of cobalt and 0.25—5 parts by weight of zirconium, titanium or chromium per 100 parts by weight of silica and prepared by impregnating a silica carrier with one or more aqueous solutions of salts of cobalt and zirconium, titanium or chromium, followed by drying the composition, calcining at 350—700°C and reducing at 200—350°C, with the proviso that if the feed has an H₂/CO molar ratio of less than 1.5, water is added to said feed and that the Co-impregnation catalyst is used in combination with a CO-shift catalyst, and that of the reaction product of the first stage at least that part the initial boiling point of which is higher than the final boiling point of the heaviest middle distillate required as final product is subjected in a second stage to a catalytic hydrotreatment. 15
2. A process as claimed in claim 1, characterized in that water is added to the H₂- and CO-containing mixture that is available as feed for the first stage, that the water-containing mixture is contacted with a CO-shift catalyst and that the mixture prepared over the CO-shift catalyst is converted over the Co-impregnation catalyst without CO₂ being removed. 25
3. A process as claimed in claim 1 or 2, characterized in that an H₂- and CO-containing mixture, to which water has been added, is contacted in the first stage either with a catalyst bed built up of several alternating layers of consecutively CO-shift catalyst and a Co-impregnation catalyst, or a physical mixture of a CO-shift catalyst and a Co-impregnation catalyst. 30
4. A process as claimed in any one of claims 1—3, characterized in that as feed for the first stage an H₂- and CO-containing fraction is used which is separated from a reaction product obtained by contacting an H₂/CO mixture (1) with an H₂/CO molar ratio of less than 2.0 with a bifunctional catalyst combination containing one or more metal components with catalytic activity for the conversion of an H₂/CO mixture into acyclic hydrocarbons and/or acyclic oxygen-containing hydrocarbons and a crystalline silicate, which silicate possesses the following properties after one hour's calcination in air at 500°C: 35
- a) thermally stable to a temperature above 600°C,
b) an X-ray powder diffraction pattern containing the four lines stated in table A as strongest lines 40

Table A

d(Å)	Relative intensities
11,1 ± 0,2	VS
10,0 ± 0,2	VS
3,84 ± 0,07	S
3,72 ± 0,06	S

where the letters used have the following meanings:

VS = very strong; S = strong

c) in the formula representing the composition of the silicate expressed in moles of oxides and

- 5 containing in addition to oxides of hydrogen, alkali metal and/or alkaline earth metal and silicon, one or more oxides of a trivalent metal A chosen from the group consisting of aluminium, iron, gallium, rhodium, chromium and scandium, the $\text{SiO}_2/\text{A}_2\text{O}_3$ molar ratio is more than 10, with the proviso that if the H_2/CO mixture (1) has an H_2/CO molar ratio of less than 1,5, a trifunctional catalyst combination is used containing one or more metal components with catalytic activity for the conversion of an H_2/CO mixture into acyclic hydrocarbons and/or acyclic oxygen-containing hydrocarbons, one or more metal components with CO-shift activity and the crystalline silicate. 5

- 10 5. A process as claimed in claim 4, characterized in that the H_2/CO mixture (1) is converted under the following conditions over the crystalline silicate-containing bi- or trifunctional catalyst combinations: a temperature of 200—500°C, a pressure of 1—150 bar and a space velocity of 10

- 15 50—5000 NI of gas/l of catalyst/h. 15

- 20 6. A process as claimed in any one of claims 1—3, characterized in that as feed for the first stage an H_2 - and CO-containing fraction is used which is separated from a reaction product obtained by contacting an H_2/CO mixture (2) having an H_2/CO molar ratio of less than 1,0 with an iron-containing bifunctional catalyst or catalyst combination possessing CO-shift activity in addition to activity for the 20 conversion of an H_2/CO mixture into substantially hydrocarbons. 20

- 25 7. A process as claimed in claim 6, characterized in that use is made of a bifunctional catalyst prepared by impregnation and containing iron supported on a carrier. 25

8. A process as claimed in any one of claims 1—7, characterized in that the second stage is carried out by contacting the feed with a catalyst containing one or more metals with hydrogenation 25 activity supported on a carrier at elevated temperature and pressure in the presence of hydrogen. 25

9. A process as claimed in claim 8, characterized in that in the second stage a catalyst is used containing one or more noble metals of Group VIII supported on a carrier. 30

10. A process as claimed in claim 9, characterized in that in the second stage a catalyst is used containing 0,1—2% by weight of one or more noble metals of Group VIII supported on a carrier comprising 13—15% by weight of alumina, the remainder consisting of silica. 30

THIS PAGE BLANK USPTO